

# Heat and Mass Transfer Effects on Unsteady MHD Radiative Flow of a Chemically Reacting Fluid Past an Impulsively Started Vertical Plate

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**Abstract** The interaction of free convection with thermal radiation of viscous incompressible MHD unsteady chemical reacting fluid flow past an impulsively started vertical plate is analyzed. The Rosseland approximation is used to describe the radiative heat transfer in the limit of the optically thin fluid. The non-linear, coupled equations are solved using an implicit finite difference scheme of Crank-Nicolson type. Velocity, temperature and concentration of the flow have been presented for various parameters such as thermal Grashof number, mass Grashof number, Prandtl number, Schmidt number, radiation parameter and magnetic parameter. The local and average skin friction, Nusslet number and Sherwood number are also presented graphically. It is observed that, when the radiation parameter increases the velocity and temperature decrease in the boundary layer. Also, it is found that the presence of chemical reaction parameter leads to decrease in the velocity field and concentration and rise in the thermal boundary thickness.

**Keywords** Heat transfer; MHD; Radiation; Finite-difference Scheme; Vertical plate.

**2010 Mathematics Subject Classification** 74A15

## 1 Introduction

Magnetohydrodynamics (MHD) is the study of the interaction of conducting fluids with electromagnetic phenomena. The flow of an electrically conducting fluid in the presence of a magnetic field is of importance in various areas of technology and engineering such as MHD power generation, MHD flow meters, MHD pumps, etc. studied the heat and mass transfer along a vertical plate under the combined buoyancy Soundalgekar et al. [1] analyzed the problem of free convection effects on Stokes problem for a vertical plate under the action of transversely applied magnetic field. Elbashbeshy [2] effects of thermal and species diffusion, in the presence of magnetic field. Helmy [3] presented an unsteady two-dimensional laminar free convection flow of an incompressible, electrically conducting (Newtonian or polar) fluid through a porous medium bounded by an infinite vertical plane surface of constant temperature.

Many transport process exist in nature and in industrial applications in which the simultaneous heat and mass transfer occur as a result of combined buoyancy effects of diffusion of chemical species. A few representative fields of interest in which combined heat and mass transfer plays an important role are designing of chemical processing equipment, formation and dispersion of fog, distribution of temperature and moisture over agricultural fields and groves of fruit trees, crop damage due to freezing, and environmental pollution. In this context the first systematic study of mass transfer effects on free convection flow past a

semi-infinite vertical plate was presented by Gebhart and Pera [4], who presented a similarity solution to this problem and introduced a parameter  $N$  which is a measure of relative importance of chemical and thermal diffusion in causing the density difference that drives the flow. The parameter  $N$  is positive when both effects combined to drive the flow and it is negative when these effects are opposed. Callahan and Marner [5] first studied the transient free convection flow past a semi-infinite plate by explicit finite difference method. They also considered the presence of species concentration. However this analysis is not applicable for fluids whose Prandtl numbers are different from unity. Soundalgekar and Ganesan [6] solved the problem of transient free convective flow past a semi-infinite vertical flat plate, taking into account mass transfer by an implicit finite difference method of Crank-Nicolson type. In their analysis they observed that an increase in  $N$  leads to an increase in the velocity but a decrease in the temperature and concentration. Muthucumarswamy and Ganesan [7] solved the problem of unsteady flow past an impulsively started semi-infinite vertical plate with heat and mass transfer.

The role of thermal radiation is of major importance in some industrial applications such as glass production and furnace design and in space technology applications, such as cosmical flight aerodynamics rocket, propulsion systems, plasma physics and space craft reentry aerothermodynamics which operate at high temperatures. When radiation is taken into account, the governing equations become quite complicated and hence many difficulties arise while solving such equations. Greif et al. [8] shown that in the optically thin limit the physical situation can be simplified, and then they derived exact solution to fully developed vertical channel for a radiative fluid. Hossain and Takhar [9] studied the radiation effects on mixed convection along a vertical plate with uniform surface temperature using Keller Box finite difference method. Abd El-Naby et al. [10] studied the effects of radiation on unsteady free convective flow past a semi-infinite vertical plate with variable surface temperature using Crank-Nicolson finite difference method. They observed that, both the velocity and temperature are found to decrease with an increase in the temperature exponent. Chamkha et al. [11] analyzed the effects of radiation on free convection flow past a semi-infinite vertical plate with mass transfer, by taking into account the buoyancy ratio parameter  $N$ . In their analysis they found that, as the distance from the leading edge increases, both the velocity and temperature decrease, whereas the concentration increases.

The radiation and mass transfer effects on unsteady MHD free convection flow past a moving vertical cylinder was studied by Gnaneswara Reddy and Bhaskar Reddy [12]. Very recently, Gnaneswara Reddy [13] presented the chemically reactive species and radiation effects on MHD convective flow past a moving vertical cylinder.

The aim of the present paper is to study the unsteady heat and mass transfer MHD flow of a chemically reacting fluid past an impulsively started vertical plate with radiation. The equations of continuity, linear momentum, energy and species concentration, which govern the flow field are solved by using an implicit finite difference scheme of Crank-Nicolson type. The behaviour of the velocity, temperature, concentration, skin-friction, Nusselt number and Sherwood number have been discussed for variations in the governing parameters.

## 2 Mathematical Analysis

An unsteady two-dimensional laminar natural convection flow of a viscous, incompressible, radiating and chemically reacting and hydromagnetic fluid past an impulsively started ver-

tical plate is considered. The  $x$ -axis is taken along the plate in the upward direction and the  $y$ -axis is taken normal to it. Initially, it is assumed that the plate and the fluid are at the same temperature  $T'_\infty$  and concentration level  $C'_\infty$  everywhere in the fluid. At time  $t' > 0$ , the plate starts moving impulsively in the vertical direction with constant velocity  $u_0$  against the gravitational field. Also, the temperature of the plate and the concentration level near the plate are raised to  $T'_w$  and  $C'_w$  respectively and are maintained constantly thereafter. It is assumed that the concentration  $C'$  of the diffusing species in the binary mixture is very less in comparison to the other chemical species, which are present, and hence the Soret and Dufour effects are negligible. Then, under the above assumptions, the governing boundary layer equations with Boussinesq's approximation are

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \quad (1)$$

$$\frac{\partial u}{\partial t'} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = g\beta(T' - T'_\infty) + g\beta^*(C' - C'_\infty) + \nu \frac{\partial^2 u}{\partial y^2} - \frac{\sigma B_0^2}{\rho} u, \quad (2)$$

$$\frac{\partial T'}{\partial t'} + u \frac{\partial T'}{\partial x} + v \frac{\partial T'}{\partial y} = \alpha \frac{\partial^2 T'}{\partial y^2} - \frac{1}{\rho c_p} \frac{\partial q_r}{\partial y}, \quad (3)$$

$$\frac{\partial C'}{\partial t'} + u \frac{\partial C'}{\partial x} + v \frac{\partial C'}{\partial y} = D \frac{\partial^2 C'}{\partial y^2} - k_l C'. \quad (4)$$

The initial and boundary conditions are

$$\begin{aligned} t' \leq 0 : u = 0, \quad v = 0, \quad T' = T'_\infty, \quad C' = C'_\infty, \\ t' > 0 : u = u_0, \quad v = 0, \quad T' = T'_w, \quad C' = C'_w \quad \text{at } y = 0, \\ u = 0, \quad T' = T'_\infty, \quad C' = C'_\infty \quad \text{at } x = 0, \\ u \rightarrow 0, \quad T' \rightarrow T'_\infty, \quad C' \rightarrow C'_\infty \quad \text{as } y \rightarrow \infty. \end{aligned} \quad (5)$$

By using the Rosseland approximation (Brewster [14]), the radiative heat flux  $q_r$  is given by

$$q_r = -\frac{4\sigma_s}{3k_e} \frac{\partial T'^4}{\partial y} \quad (6)$$

where  $\sigma_s$  is the Stefan-Boltzmann constant and  $k_e$  - the mean absorption coefficient. It should be noted that by using the Rosseland approximation the present analysis is limited to optically thick fluids. If temperature differences within the flow are sufficiently small, then Equation (6) can be linearized by expanding  $T'^4$  into the Taylor series about  $T'_\infty$ , which after neglecting higher order terms takes the form

$$T'^4 \cong 4T'_\infty{}^3 T' - 3T'_\infty{}^4. \quad (7)$$

In view of Equations (6) and (7), Equation (3) reduces to

$$\frac{\partial T'}{\partial t'} + u \frac{\partial T'}{\partial x} + v \frac{\partial T'}{\partial y} = \alpha \frac{\partial^2 T'}{\partial y^2} + \frac{16\sigma_s T'_\infty{}^3}{3k_e \rho c_p} \frac{\partial^2 T'}{\partial y^2}. \quad (8)$$

Local and average skin-friction are given respectively by

$$\tau'_x = -\mu \left( \frac{\partial u}{\partial y} \right)_{y=0}, \quad (9)$$

$$\bar{\tau}_L = \frac{-1}{L} \int_0^L \mu \left( \frac{\partial u}{\partial y} \right)_{y=0} dx. \quad (10)$$

Local and average Nusselt number are given respectively by

$$Nu_x = \frac{-x \left( \frac{\partial T'}{\partial y} \right)_{y=0}}{T'_w - T'_\infty}, \quad (11)$$

$$\overline{Nu}_L = - \int_0^L \left[ \left( \frac{\partial T'}{\partial y} \right)_{y=0} / (T'_w - T'_\infty) \right] dx. \quad (12)$$

Local and average Sherwood number are given respectively by

$$Sh_x = \frac{-x \left( \frac{\partial C'}{\partial y} \right)_{y=0}}{C'_w - C'_\infty}, \quad (13)$$

$$\overline{Sh}_L = - \int_0^L \left[ \left( \frac{\partial C'}{\partial y} \right)_{y=0} / (C'_w - C'_\infty) \right] dx. \quad (14)$$

On introducing the following non-dimensional quantities

$$\begin{aligned} X &= \frac{x u_0}{\nu}, \quad Y = \frac{y u_0}{\nu}, \quad t = \frac{t' u_0^2}{\nu}, \quad U = \frac{u}{u_0}, \quad V = \frac{v}{u_0}, \quad M = \frac{\sigma B_0^2 \nu}{u_0^2}, \\ Gr &= \frac{\nu g \beta (T'_w - T'_\infty)}{u_0^3}, \quad Gc = \frac{\nu g \beta^* (C'_w - C'_\infty)}{u_0^3}, \quad N = \frac{k_e k}{4\sigma_s T'_\infty{}^3}, \\ T &= \frac{T' - T'_\infty}{T'_w - T'_\infty}, \quad C = \frac{C' - C'_\infty}{C'_w - C'_\infty}, \quad Pr = \frac{\nu}{\alpha}, \quad Sc = \frac{\nu}{D}, \quad K = \frac{K_l \nu}{u_0^2}. \end{aligned} \quad (15)$$

Equations (1), (2), (8) and (4) are reduced to the following non-dimensional form

$$\frac{\partial U}{\partial X} + \frac{\partial V}{\partial Y} = 0, \quad (16)$$

$$\frac{\partial U}{\partial t} + U \frac{\partial U}{\partial X} + V \frac{\partial U}{\partial Y} = Gr T + Gc C + \frac{\partial^2 U}{\partial Y^2} - MU, \quad (17)$$

$$\frac{\partial T}{\partial t} + U \frac{\partial T}{\partial X} + V \frac{\partial T}{\partial Y} = \frac{1}{Pr} \left( 1 + \frac{4}{3N} \right) \frac{\partial^2 T}{\partial Y^2}, \quad (18)$$

$$\frac{\partial C}{\partial t} + U \frac{\partial C}{\partial X} + V \frac{\partial C}{\partial Y} = \frac{1}{Sc} \frac{\partial^2 C}{\partial Y^2} - KC. \quad (19)$$

The corresponding initial and boundary conditions are

$$\begin{aligned} t \leq 0 : U &= 0, \quad V = 0, \quad T = 0, \quad C = 0, \\ t > 0 : U &= 1, \quad V = 0, \quad T = 1, \quad C = 1 && \text{at } Y = 0, \\ U &= 0, \quad T = 0, \quad C = 0 && \text{at } X = 0, \\ U &\rightarrow 0, \quad T \rightarrow 0, \quad C \rightarrow 0 && \text{as } Y \rightarrow \infty. \end{aligned} \quad (20)$$

where  $Gr$  is the thermal Grashof number,  $Gc$  - the solutal Grashof number,  $M$ - the magnetic field parameter,  $Pr$  - the fluid Prandtl number,  $Sc$  - the Schmidt number and  $N$  - the radiation parameter,  $K$ - the chemical reaction parameter.

Local and average skin-friction in non-dimensional form are

$$\tau_X = \frac{\tau'}{\rho u_0^2} = - \left( \frac{\partial U}{\partial Y} \right)_{Y=0}, \quad (21)$$

$$\bar{\tau} = - \int_0^1 \left( \frac{\partial U}{\partial Y} \right)_{Y=0} dX. \quad (22)$$

Local and average Nusselt number in non-dimensional form are

$$Nu_X = -X \left( \frac{\partial T}{\partial Y} \right)_{Y=0} \quad (23)$$

$$\overline{Nu} = - \int_0^1 \left( \frac{\partial T}{\partial Y} \right)_{Y=0} dX. \quad (24)$$

Local and average Sherwood number in non-dimensional form are

$$Sh_X = -X \left( \frac{\partial C}{\partial Y} \right)_{Y=0}, \quad (25)$$

$$\overline{Sh} = - \int_0^1 \left( \frac{\partial C}{\partial Y} \right)_{Y=0} dX. \quad (26)$$

### 3 Numerical Technique

In order to solve the unsteady, non-linear coupled Equations (16) - (19) under the conditions (20), an implicit finite difference scheme of Crank-Nicolson type has been employed. The region of integration is considered as a rectangle with sides  $X_{\max}(=1)$  and  $Y_{\max}(=14)$ , where  $Y_{\max}$  corresponds to  $Y = \infty$ , which lies very well outside the momentum, energy and concentration boundary layers. The maximum of  $Y$  was chosen as 14 after some preliminary investigations, so that the last two of the boundary conditions (20) are satisfied within the tolerance limit  $10^{-5}$ .

The finite difference equations corresponding to Equations (16) - (19) are as follows

$$\frac{[U_{i,j}^{n+1} - U_{i-1,j}^{n+1} + U_{i,j}^n - U_{i-1,j}^n + U_{i,j-1}^{n+1} - U_{i-1,j-1}^{n+1} + U_{i,j-1}^n - U_{i-1,j-1}^n]}{4\Delta X} + \frac{[V_{i,j}^{n+1} - V_{i,j-1}^{n+1} + V_{i,j}^n - V_{i,j-1}^n]}{2\Delta Y} = 0, \quad (27)$$

$$\begin{aligned}
& \frac{[U_{i,j}^{n+1} - U_{i,j}^n]}{\Delta t} + U_{i,j}^n \frac{[U_{i,j}^{n+1} - U_{i-1,j}^{n+1} + U_{i,j}^n - U_{i-1,j}^n]}{2\Delta X} + \\
& V_{i,j}^n \frac{[U_{i,j+1}^{n+1} - U_{i,j-1}^{n+1} + U_{i,j+1}^n - U_{i,j-1}^n]}{4\Delta Y} \\
& = Gr \frac{[T_{i,j}^{n+1} + T_{i,j}^n]}{2} + Gc \frac{[C_{i,j}^{n+1} + C_{i,j}^n]}{2} + \\
& \frac{[U_{i,j-1}^{n+1} - 2U_{i,j}^{n+1} + U_{i,j+1}^{n+1} + U_{i,j-1}^n - 2U_{i,j}^n + U_{i,j+1}^n]}{2(\Delta Y)^2} - \frac{M}{2} [U_{i,j}^{n+1} + U_{i,j}^n], \quad (28)
\end{aligned}$$

$$\begin{aligned}
& \frac{[T_{i,j}^{n+1} - T_{i,j}^n]}{\Delta t} + U_{i,j}^n \frac{[T_{i,j}^{n+1} - T_{i-1,j}^{n+1} + T_{i,j}^n - T_{i-1,j}^n]}{2\Delta X} + V_{i,j}^n \frac{[T_{i,j} - T_{i,j-1}^{n+1} + T_{i,j+1}^n - T_{i,j-1}^n]}{4\Delta Y} \\
& = \frac{1}{Pr} \left( 1 + \frac{4}{3N} \right) \frac{[T_{i,j-1}^{n+1} - 2T_{i,j}^{n+1} + T_{i,j+1}^{n+1} + T_{i,j-1}^n - 2T_{i,j}^n + T_{i,j+1}^n]}{2(\Delta Y)^2}, \quad (29)
\end{aligned}$$

$$\begin{aligned}
& \frac{[C_{i,j}^{n+1} - C_{i,j}^n]}{\Delta t} + U_{i,j}^n \frac{[C_{i,j}^{n+1} - C_{i-1,j}^{n+1} + C_{i,j}^n - C_{i-1,j}^n]}{2\Delta X} + \\
& V_{i,j}^n \frac{[C_{i,j+1}^{n+1} - C_{i,j-1}^{n+1} + C_{i,j+1}^n - C_{i,j-1}^n]}{4\Delta Y} \\
& = \frac{1}{Sc} \frac{[C_{i,j-1}^{n+1} - 2C_{i,j}^{n+1} + C_{i,j+1}^{n+1} + C_{i,j-1}^n - 2C_{i,j}^n + C_{i,j+1}^n]}{2(\Delta Y)^2} - \frac{K}{2} [C_{i,j}^{n+1} + C_{i,j}^n]. \quad (30)
\end{aligned}$$

Here, the subscript  $i$  - designates the grid point along the X - direction,  $j$  - along the Y-direction and the superscript  $n$  along the  $t$  - direction. An appropriate mesh size considered for the calculation is  $\Delta X = 0.05$ ,  $\Delta Y = 0.25$ , and time step  $\Delta t = 0.01$ . During any one-time step, the coefficients  $U_{i,j}^n$  and  $V_{i,j}^n$  appearing in the difference equations are treated as constants. The values of  $U, V, T$  and  $C$  are known at all grid points at  $t = 0$  from the initial conditions. The computations of  $U, V, T$  and  $C$  at time level  $(n + 1)$  using the known values at previous time level  $(n)$  are calculated as follows.

The finite difference Equation (30) at every internal nodal point on a particular  $i$ - level constitute a tri-diagonal system of equations. Such a system of equations is solved by Thomas algorithm as described in Carnahan et al. [15]. Thus, the values of  $C$  are found at every nodal point on a particular  $i$  at  $(n+1)^{\text{th}}$  time level . Similarly, the values of  $T$  are calculated from the Equation (29). Using the values of  $C$  and  $T$  at  $(n+1)^{\text{th}}$  time level in the Equation (28), the values of  $U$  at  $(n+1)^{\text{th}}$  time level are found in a similar manner. Thus the values of  $C, T$  and  $U$  are known on a particular  $i$  - level. The values of  $V$  are calculated explicitly using the Equation (27) at every nodal point on a particular  $i$ - level at  $(n+1)^{\text{th}}$  time level. This process is repeated for various  $i$ - levels. Thus, the values of  $C, T, U$  and  $V$  are known at all grid points in the rectangular region at  $(n+1)^{\text{th}}$  time level.

Computations are carried out till the steady state is reached. The steady state solution is assumed to have been reached, when the absolute difference between the values of  $U$  as well as temperature  $T$  and concentration  $C$  at two consecutive time steps are less than  $10^{-5}$  at all grid points. The derivatives involved in the Equations (21) - (26) are evaluated using five-point approximation formula and the integrals are evaluated using Newton-Cotes closed integration formula.

## 4 Results and Discussion

A representative set of numerical results is shown graphically in Figures.1-10, to illustrate the influence of physical parameters viz., radiation parameter  $N$ , Grashof number  $Gr$ , mass Grashof number  $Gc$ , Magnetic field parameter  $M$ , Schmidt number  $Sc$  and chemical reaction parameter  $K$  on the velocity, temperature and concentration, skin-friction, Nusselt number and Sherwood number. The value of the Prandtl number  $Pr$  is chosen to be 0.71 (i.e., for air) and the other parameters are arbitrarily chosen.

The transient velocity profiles for different values of  $Gr$ ,  $Gc$ ,  $M$ ,  $N$ ,  $Sc$  and  $K$  at a particular time  $t = 1.0$  has been shown in Figure 1. It is observed that the transient velocity increases with the increase in  $Gr$  or  $Gc$ . There is a fall in transient velocity with the increase in  $M$ ,  $N$ ,  $Sc$  or  $K$ . In Figure 2, the transient and steady state velocity profiles are presented for different values  $M, N, Sc, K$  and the buoyancy force parameters  $Gr$  or  $Gc$ . The steady state velocity increases with the increase in  $Gr$  or  $Gc$ . The time required to reach the steady state and the velocity decreases with the increase in  $M, N, Sc$  and  $K$ . Figure 3 shows the temperature decreases with the increasing values of  $Gr$  or  $Gc$ . It can also be seen that the time required to reach the steady state temperature is more at higher values of  $N (=10)$ , as compared to lower values of  $N (=5)$ . From Figures 1 to 3, it is observed that, owing to an increase in the value of radiation parameter  $N$ , the velocity and temperature decrease accompanied by simultaneous reductions in both momentum and thermal boundary layers. However the time taken to reach the steady state increases as  $N$  increases. The transient concentration profiles for  $Pr = 0.71$ ,  $Gr = Gc (=2)$ ,  $N = 5, 10$  and  $Sc = 0.6$  and  $2.0$  are shown in Figure 4. It is observed that for small values of  $Sc = 0.6$ ,  $K = 0.5$  and  $N = 5$ , the time required to reach the steady state is 8.10, where as when  $N = 10$ , under similar conditions, the time required to reach the steady state is 8.31 from which it is concluded that for higher values of  $N$ , the time taken to reach the steady state is more when  $Sc$  is small. It is also observed that increasing values of  $N$  corresponds to a thicker concentration boundary layer relative to the momentum boundary layer. Hence, it can be noted that at larger  $Sc$ , the time required to reach the steady state is less as compared to that at low values of  $Sc$ . Also, an increase in  $Sc$  or  $K$  leads to a fall in concentration.

Steady state local skin-friction  $\tau_X$  profiles are shown in Figure 5. The local shear stress  $\tau_X$  increases with the increase in  $Sc$  or  $K$ , where as it decreases with the increase in  $Gr$  or  $Gm$ . It is also observed that the local skin-friction  $\tau_X$  increases as the radiation parameter  $N$  increases. The average values of skin-friction  $\bar{\tau}$  are plotted in Figure 6. It is observed that decreases with the increase in  $Gr$  or  $Gm$  throughout the transient period and at the steady state level. It is also observed that the average skin-friction  $\bar{\tau}$  increases as the radiation parameter  $N$  increases. The average skin-friction increases with increasing  $Sc$  or  $K$ . The local Nusslet number  $Nu_X$  for different  $Gr$ ,  $Gm$ ,  $N$ ,  $Sc$  and  $K$  are shown in Fig.7. The local heat transfer rate  $Nu_X$  decreases with the increase in  $Sc$  or  $K$ , whereas it increases with the increase in  $Gr$  or  $Gm$ . Also it is found that as the radiation parameter  $N$  increases the local Nusselt number  $Nu_X$  increases. The average values of Nusselt number  $\overline{Nu}$  are shown in Figure 8. It is noticed that the average Nusselt number  $\overline{Nu}$  increases with the increase in  $Gr$  or  $Gm$  or  $N$ , whereas it increases with the decrease in  $Sc$  or  $K$ . The local Sherwood number  $Sh_X$  is plotted in Figure 9. It is observed that  $Sh_X$  increases with the increase in  $Sc$  or  $K$ , where as it decreases with the increase in  $Gr$ ,  $Gm$  or  $N$ . The average values of Sherwood number  $\overline{Sh}$  are plotted in Figure 10. It is seen that average Sherwood number  $\overline{Sh}$  increases with the increase in  $Gr$  or  $Gm$  or  $N$ .

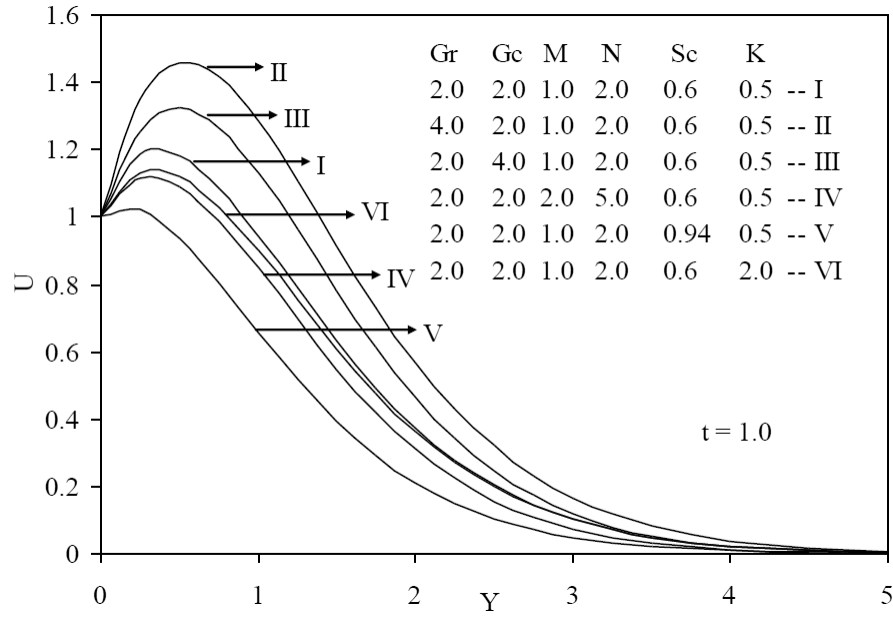


Figure 1: Transient Velocity Profiles at  $X = 1.0$  for Different  $Gr, Gc, M, N, Sc,$

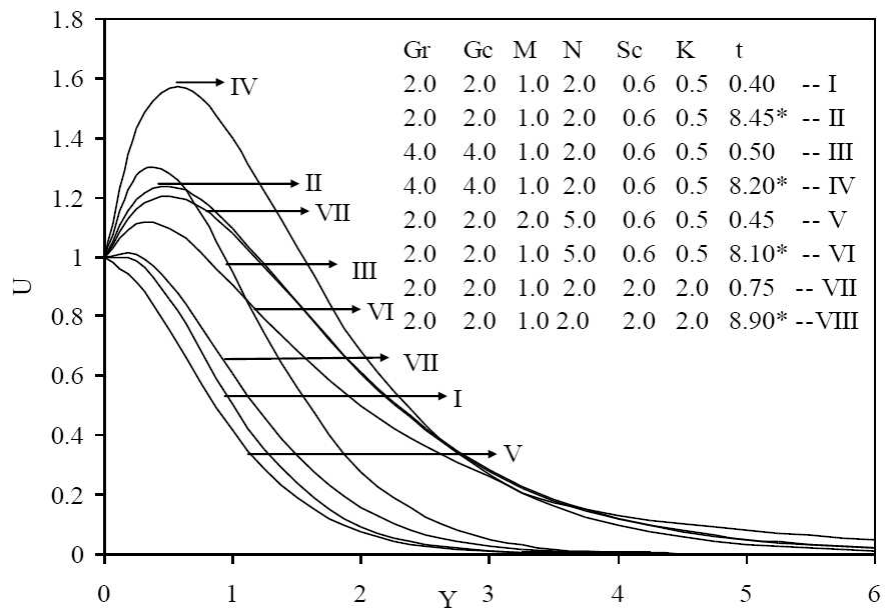


Figure 2: Velocity Profiles at  $X = 1.0$  for Different  $Gr, Gc, N, Sc$  and  $K$



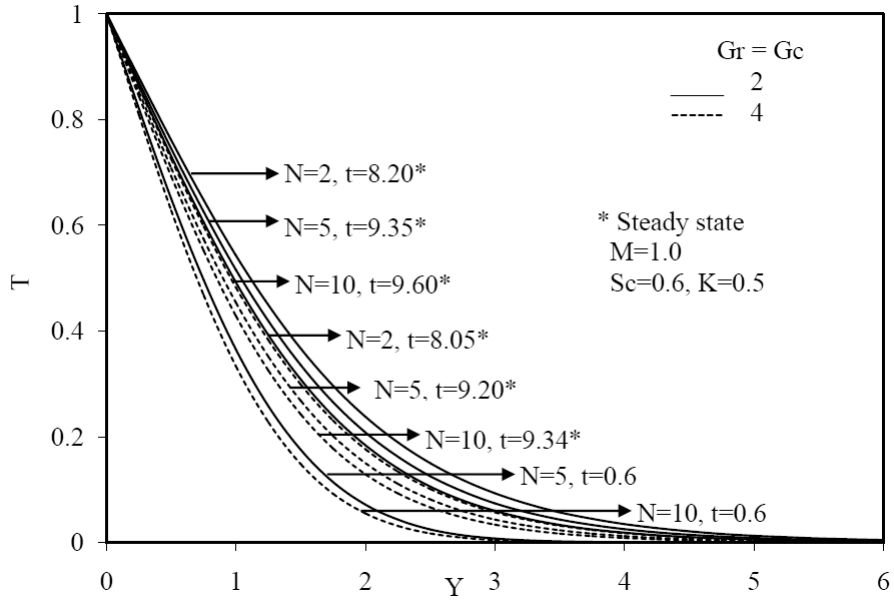


Figure 3: Temperature Profiles at  $X = 1.0$  for Different  $Gr, Gc, N$

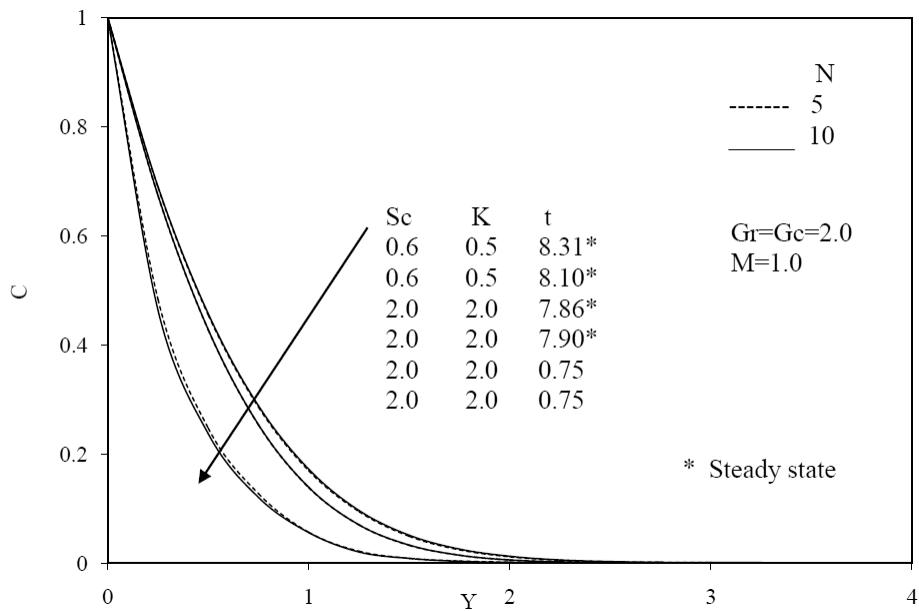


Figure 4: Concentration Profiles at  $X = 1.0$  for Different  $Sc$  and  $K$

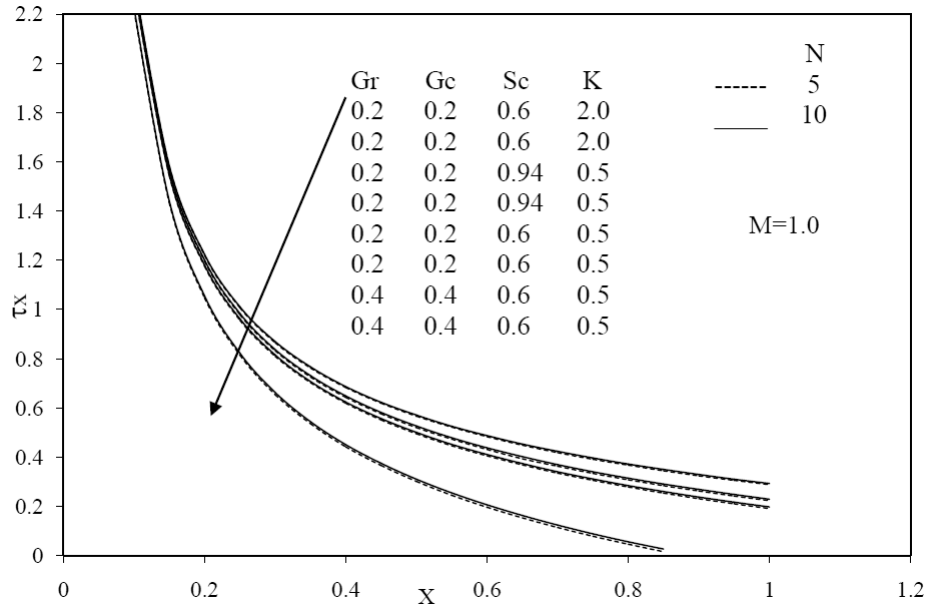


Figure 5: Local Skin-friction

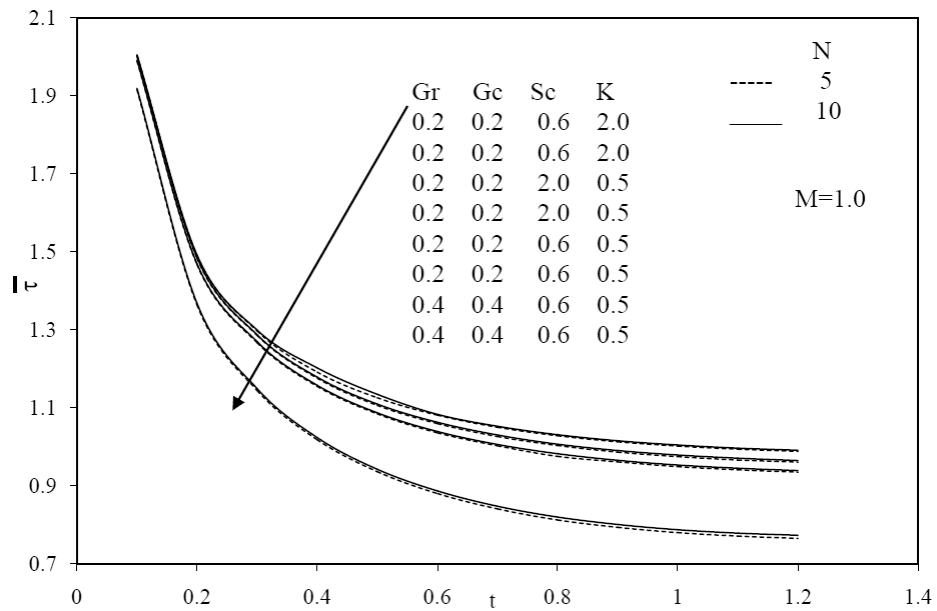


Figure 6: Average Skin-friction

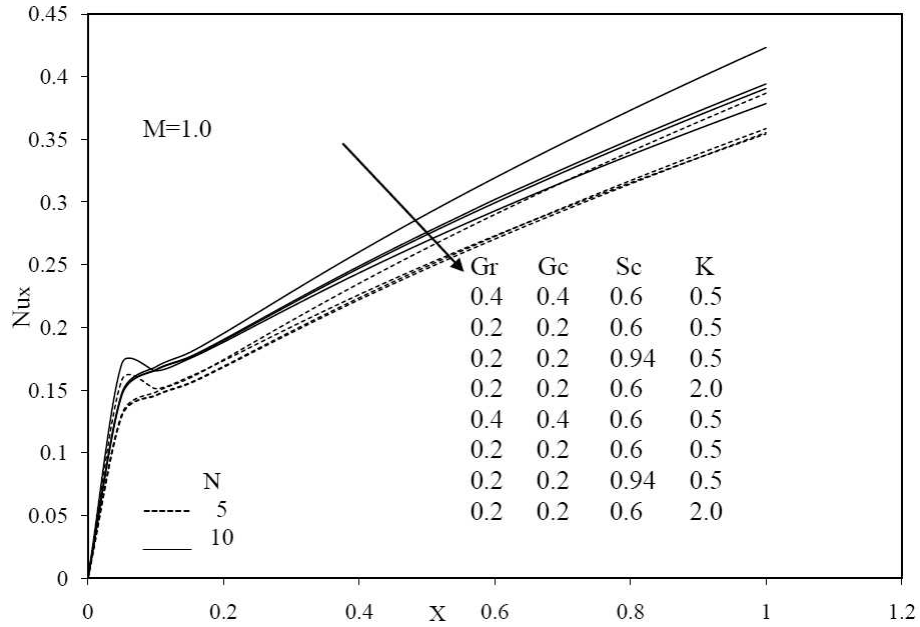


Figure 7: Local Nusselt Number

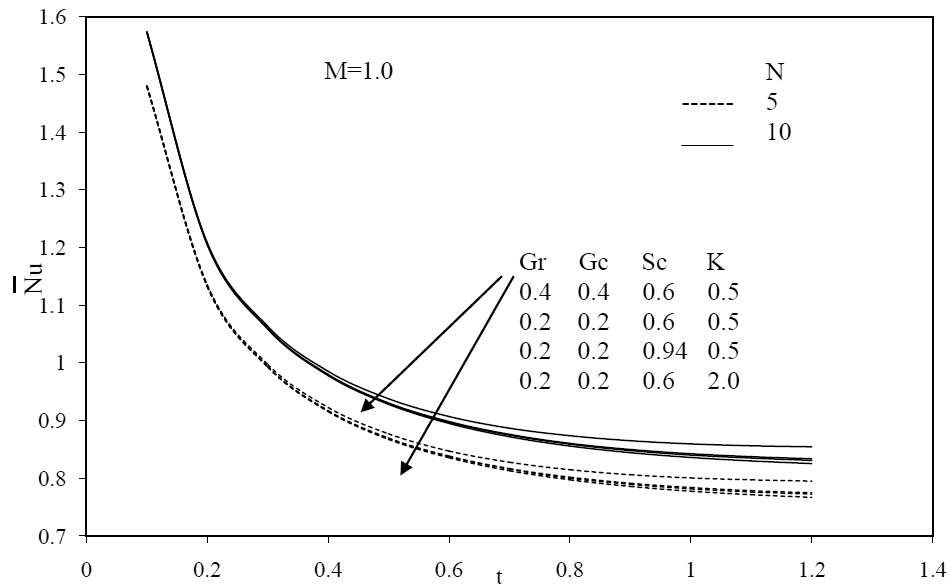


Figure 8: Average Nusselt Number

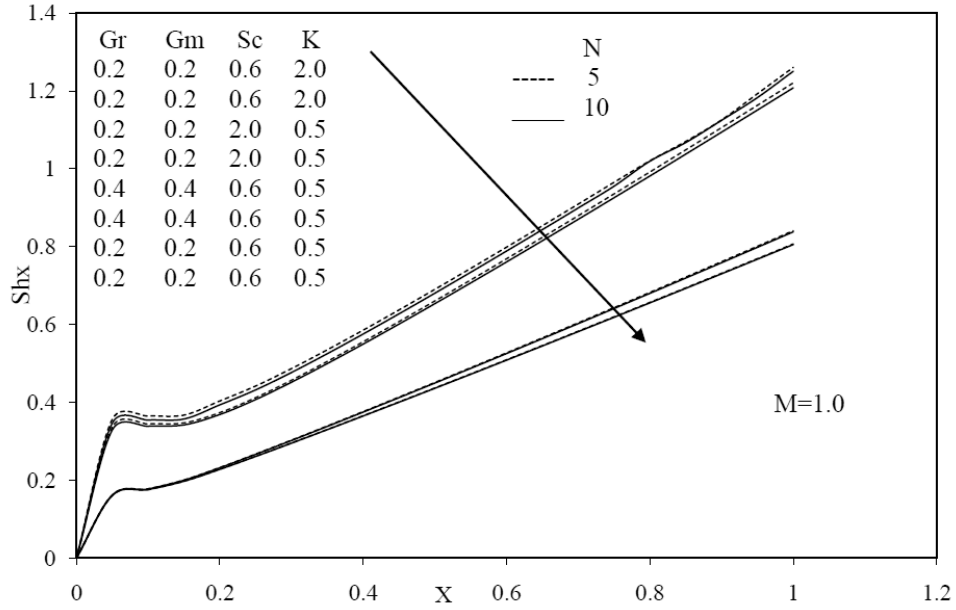


Figure 9: Local Sherwood Number

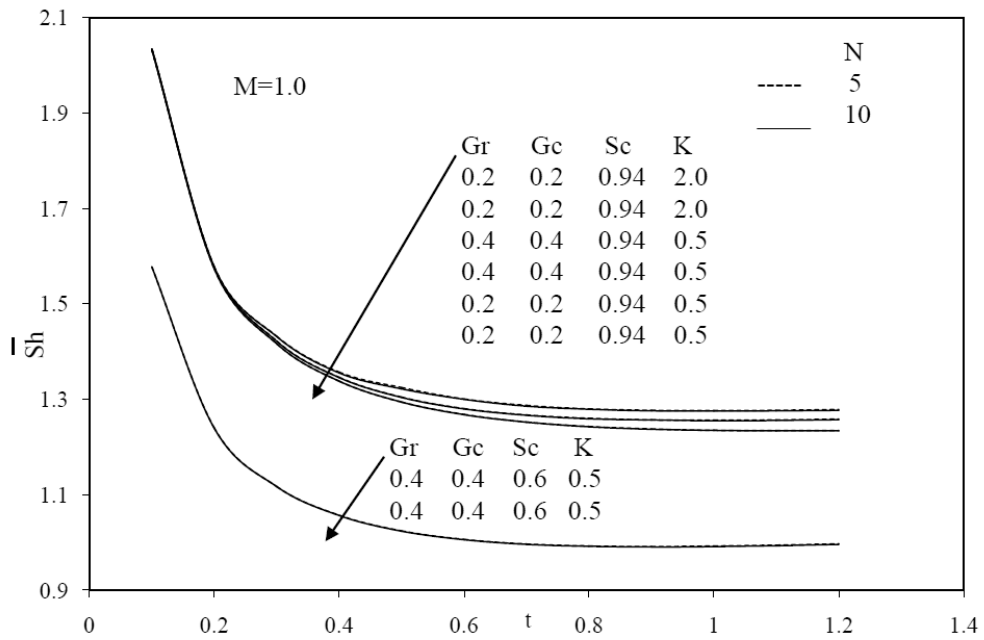


Figure 10: Average Sherwood Number

## 5 Conclusions

A detailed numerical study has been carried out for the radiative MHD chemically reacting fluid flow past an impulsively started vertical plate. The dimensionless governing equations are solved by an implicit finite-difference method of Crank-Nicolson type. Conclusions of the study are as follows.

- (i) The magnetic field parameter has retarding effect on the velocity.
- (ii) At small values of the radiation parameter  $N$ , the velocity and temperature of the fluid increases sharply near the plate as the time  $t$  increase.
- (iii) The velocity and concentration field is decrease as the chemical reaction parameter increases.
- (iv) The skin-friction decreases with an increase  $M$  and increases with the increasing value of radiation parameter  $N$  and chemical reaction parameter  $K$  or Schmidt number  $Sc$ .

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### List of Symbols

$B_0$	the magnetic induction
$C'$	concentration
$C$	dimensionless concentration
$Gr$	thermal Grashof number
$Gc$	modified Grashof number
$g$	acceleration due to gravity
$K$	chemical reaction parameter
$M$	magnetic parameter
$N$	radiation parameter
$\overline{Nu}$	average Nusselt number
$Nu_x$	local Nusselt number
Pr	Prandtl number
$q_r$	radiative heat flux
$Sc$	Schmidt number
$\overline{Sh}$	average Sherwood number
$Sh_x$	local Sherwood number
$T'$	temperature
$T$	dimensionless temperature
$t'$	time
$t$	dimensionless time
$u_0$	velocity of the plate
$U, V$	dimensionless velocity components in $X, R$ directions respectively
$x$	spatial coordinate along the plate
$X$	dimensionless spatial coordinate along the plate
$y$	spatial coordinate normal to the plate
$Y$	dimensionless spatial coordinate normal to the plate

**Greek Symbols**

$\alpha$	thermal diffusivity
$\beta$	volumetric coefficient of thermal expansion
$\beta^*$	volumetric coefficient of expansion with concentration
$k_e$	mean absorption coefficient
$\nu$	kinematic viscosity
$\rho$	density
$\sigma$	electrical conductivity
$\sigma_s$	Stefan-Boltzmann constant
$\tau_x$	local skin-friction
$\bar{\tau}$	average skin-friction

**Subscripts**

$w$	condition on the wall
$\infty$	free stream condition